

Permeability of a packed bed



Inertia: Darcy-Forchheimer's law.

\vec{v} : grad $\vec{v} \rightarrow$ inertia term

Homogenization

$$\hookrightarrow \text{grad} \langle \vec{v} \rangle = -\eta \bar{K}^{-1} \langle \vec{v} \rangle - \langle \beta \rangle \langle \vec{v} \rangle$$

$\rightarrow \beta$ depends only on the porous media.

$$\rightarrow \langle \vec{v} \rangle = -\text{grad} \langle \psi \rangle \bar{K} - \langle \beta \rangle \langle \vec{v} \rangle$$

$$\langle \vec{v} \rangle (1 + \langle \beta \rangle \|\bar{K}\|) = -\text{grad} \langle \psi \rangle \bar{K}$$

$$\langle \vec{v} \rangle = -\frac{\bar{K}_{\text{eff}}}{\eta} \text{grad} \langle \psi \rangle$$

with $\bar{K}_{\text{eff}} = \frac{\bar{K}}{1 - \epsilon \langle \beta \rangle \|\bar{K}\|}$

where $\langle \beta \rangle = \frac{\rho \sqrt{\bar{K}} \|\bar{K}\|}{\eta \epsilon}$

$$\bar{K}_{\text{eff}} = f(\|\bar{K}\|)$$

Erjen's law

\hookrightarrow Packed bed

n cylinders (length L , diameter D)

$$\Rightarrow \text{Poiseuille} \Rightarrow \frac{\Delta P}{L} = \frac{32 \eta L \langle \vec{v} \rangle}{D^4}$$

average velocity through the P.M

For a laminar flow, $\frac{\Delta P}{L} = 180 \frac{(1-\epsilon)^2 \eta U}{\epsilon^3 D_p^2}$ particle diameter.

Dimensional analysis

$$[\Delta P] = \text{J} \cdot \text{m}^{-3} = \text{kg} \cdot \text{m}^{-1} \cdot \text{s}^{-2}$$

ΔP must be proportional to kinetic energy / m^3

$$\Rightarrow \Delta P \propto L \rho \langle \vec{v} \rangle^2 \propto \frac{1}{2} \rho \frac{1}{D}$$

$$\Rightarrow \frac{\Delta P}{L} = \frac{\rho}{2D} \langle \vec{v} \rangle^2 \quad \text{contribution of inertia.}$$

Moreover, $\langle \vec{v} \rangle = \epsilon \langle \vec{v} \rangle^*$
 $U = \epsilon \langle \vec{v} \rangle^*$

furthermore $\epsilon = \frac{n}{V} L \pi \frac{D^2}{4}$
 $a = \frac{n \pi D L}{V} \Rightarrow \epsilon = a \frac{D}{4}$ cylinders.

and for a particle bed: $\epsilon = 1 - \frac{a D_p}{6}$

Now we consider that PM1 \rightarrow assembly of cylinders
 PM2 \rightarrow Packed bed

they have the same ϵ and a .

$$\frac{\Delta P}{L} = \frac{\rho}{2D} \langle \vec{v} \rangle^2 = \frac{a \rho}{8 \epsilon} \langle \vec{v} \rangle^2$$

We have the same specific surface between PM1 and PM2

$$\Rightarrow \frac{\Delta P}{L} = \frac{3 \rho (1-\epsilon)}{4 D_p \epsilon^3} U^2$$

\hookrightarrow contribution of inertia to permeability.

$$\frac{\Delta P}{L} = \underbrace{\frac{(1-\epsilon)^2 \eta}{\epsilon^3 D_p}}_{\text{laminar}} U + \underbrace{\langle \beta \rangle \frac{3(1-\epsilon) \rho}{4 \epsilon^3} \frac{\rho}{D_p}}_{\text{inertia}} U^2$$

Erjen's correlation
 \hookrightarrow tortuosity

1) Hagen-Poiseuille: $\langle \vec{v} \rangle = \frac{h^2 \Delta P}{12 \eta L}$

Darcy: $\langle \vec{v} \rangle = -\frac{K}{\eta} \text{grad} \langle \psi \rangle = \frac{\Delta P}{L}$

$$\Rightarrow K = \frac{h^2}{12}$$

2) $\epsilon = \frac{V_{\text{void}}}{V_{\text{tot}}} = \frac{V_{\text{tot}} - V_{\text{particles}}}{V_{\text{tot}}} = 1 - \frac{n \pi D^3}{6} \times \frac{1}{V}$

$a = \frac{S_{\text{particles}}}{V} = \frac{n \pi D^2}{V}$ specific surface porosity

$\Rightarrow \epsilon = 1 - \frac{a D}{6} \Leftrightarrow a = (1 - \epsilon) \frac{6}{D}$ diameter.

3) $U = \frac{\epsilon^3}{2 \tau^2 a^2} \frac{\Delta P}{\eta L} \Rightarrow k = \frac{\epsilon^3}{2 \tau^2 a^2}$

4) $k = \frac{\epsilon^3}{2 \tau^2 (1-\epsilon)^2 \frac{36}{D^2}} = \frac{D^2 \epsilon^3}{72 \tau^2 (1-\epsilon)^2}$

5) $\tau = \frac{L'}{D} = \frac{\pi D_p}{D} = \frac{\pi}{2}$

6) Kozeny-Carmen relation.

$$k = \frac{\epsilon^3 D^2}{180 \pi^2 (1-\epsilon)^2} \approx \frac{\epsilon^3 D^2}{180 (1-\epsilon)^2}$$

Kozeny-Carmen factor

depends on the real beads spatial organization.